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Process for the telomerization of conjugated alkadienes.

The process for the telomerization of conjugated alkadienes which comprises contacting a conjugated alkadiene with a compound having at least one active hydrogen atom, in the presence of a catalyst obtainable from a palladium compound and a diphosphine of general formula R¹R²PRPR³R⁴, wherein R is a bivalent organic bridging group containing at least 3 atoms in the bridge, of which at least two are carbon atoms; R¹,R²,R³ and R⁴ are the same or different and respresent optionally polar substituted hydrocarbyl groups.

The present process relates to a process for the telomerization of conjugated dienes, and more in particular to such a process conducted in the presence of a catalyst based on a palladium compound and a phosphine ligand, and to the products thus prepared.

Telomerization is a known reaction and refers to the reaction of conjugated alkadienes in the presence of a compound having an active hydrogen, such as for example a hydroxy compound, a primary or secondary amine, a carboxylic acid, a compound containing an active methylene group, and water.

The telomerization of conjugated alkadienes is known for example from Dutch Patent Specification 156 387, which document relates to the oligomerization of specified conjugated dienes in the presence of a compound containing active hydrogen and a catalyst based on a combination of a bivalent palladium compound and a phosphine or arsine. Although both mono – and diphosphines and arsines are claimed, there appears to be a strong preference for the use of monophosphines, and especially triphenyl – phosphines. In fact in all the examples the catalyst either is based on a monophosphine or a monoarsine. From the large number of examples provided it can be observed that an acceptable degree of al – kadieneconversion and/or the selectivity to the desired reaction product is only obtained when the active hydrogen containing compound employed is an organic hydroxy compound. When using other types of active hydrogen containing compounds the alkadiene conversion and selectivity leave considerable room for improvement.

As mentioned hereinbefore water is also considered to be an active hydrogen containing compound for use in telomerization reactions, as it offers the possibility of converting the alkadienes to the corresponding hydroxy dimercompounds, which compounds may be used e.g. in organic synthesis. The only information provided in said Dutch Patent Specification regarding the use of water is as a solvent.

The preparation of 2.7-octadienol-1 via a catalytic telomerization of butadiene in the presence of water is known from Russian Patent Application SU 979-316-A. Said method however, has a disadvan-tage in that it employs a rather complicated multicomponent catalyst system which comprises a specified metal sulphate, a palladium salt, a phosphine (such as an alkyl or aryl monophosphine) or a phospine and an organo-aluminium reducing agent.

It will be appreciated that the known catalyst system based on a palladium compound and a monophosphine such as for example triphenylphosphine, will be less stable and thus have a shorter life time, than similar catalyst systems containing chelating ligands such as for example 1.2 – bis – (diphenylphosphino)ethane.

Hence it can be concluded that there is considerable need for improvement in the telomerization of alkadienes. The problem underlying the present invention is to develop a process for the telomerization of alkadienes which does not suffer from one or more of the disadvantages as described hereinbefore. Thus, there is a need to develop a process for the telomerization of alkadienes which is conducted in the presence of active hydrogen – containing compounds, which combines a high alkadiene conversion with a high selectivity and/or which can be conducted in the presence of a relatively simple catalyst system.

As a result of extensive research and experimentation it was now found that the telomerization of alkadienes in the presence of an active hydrogen – containing compound could conveniently be conducted in the presence of a catalyst based on a palladium compound and selected diphosphines.

Accordingly the invention provides a process for the telomerization of conjugated alkadienes which comprises contacting a conjugated alkadiene with a compound having at least one active hydrogen atom, in the presence of a catalyst obtainable from a palladium compound and a diphosphine of general formula R¹R²PRPR³R⁴, wherein R is a bivalent organic bridging group containing at least 3 atoms in the bridge, of which at least two are carbon atoms; R¹,R²,R³ and R⁴ are the same or different and respresent optionally polar – substituted hydrocarbyl groups.

Preferably the bridging group R of the diphosphine mentioned hereinbefore contains 3 to 5 atoms in the bridge. Examples of suitable bridging groups R include $-(CH_2)_3 - , -(CH_2)_4 - , -CH_2 - C(CH_3)_2 - CH_2$ and $-CH_2 - Si(CH_3)_2 - CH_2 - .$

The hydrocarbyl groups R^1,R^2,R^3 and R^4 are preferably the same and represent an aryl group, a phenyl group being the preferred aryl group, or an alkyl group having up to 10 carbon atoms. Preferred said alkyl groups have from 2 to 5 carbon atoms and may be linear or branched as exemplified by ethyl, propyl, isopropyl, butyl, tert – butyl and pentyl. Preferred diphosphines for use in the process of the present invention are 1,3 – bis(diphenylphosphino)propane, 1,4 – bis(diphenylphosphino)propane, 1,3 – bis(diisopropylphosphino)propane, 1,3 – bis(di – n – butylphosphino)propane and 1,4 – bis(di – n – butylphosphino)butane.

The palladium compound on which the catalyst in the process of the present invention is based is preferably a palladium salt of a carboxylic acid, and palladium acetate in particular.

The conjugated alkadienes which may be converted by the process of the present invention will generally have from 4 to 8 carbon atoms and include 1,3-butadiene, isoprene, 1,3-pentadiene, 2,4-hexadiene and 2,3-dimethylbutadiene - 1,3; 1,3-butadiene is a preferred conjugated alkadiene.

A wide range of compounds having an active hydrogen such as for example alcohols, hydroxy – aromatic compounds, primary and secondary amines, carboxylic acids, compounds having an active methylene group and water, may conveniently be used in the process of the present invention. The nature of the main reaction product which may be prepared by the process of the present invention will generally comprise an adduct of the active hydrogen – containing compound and a triene which compound can considered to have been obtained by dimerization of the relevant conjugated diene. Hence the reaction product will for example be an alcohol when water has been used as the active hydrogen containing compound, an ether when an alcohol is used, a secondary or tertiary amine when respectively a primary or secondary amine is used. In general, the hereinbefore described reaction products will be present as admixtures with minor amounts of the corresponding triene. In the present process water and primary or secondary amines are the preferred active hydrogen – containing compounds.

In the process of the present invention the diphosphines are preferably used in a quantity of from 0.2 to 10 and in particular from 0.5 to 5 mol per gram atom of palladium. The palladium compound will generally be employed in an amount which corresponds with a ratio in the range of from 10^{-6} to 10^{-1} and preferably from 10^{-5} to 10^{-2} gram atom of palladium per mol of conjugated alkadiene.

The process may conveniently be conducted in the presence of one or more inert solvents and or diluents. Suitable solvents and/or diluents include ketones, such as acetone; ethers, such as dioxane, tetrahydrofuran, anisole (methyl phenyl ether) and diglyme (dimethyl ether of diethylene glycol); hydrocar – bon compounds, such as benzene, toluene, cyclohexane and n – hexane; and polar compounds such as dimethylformamide and dimethylsulfoxide. Occasionally water may also be used as a solvent or diluent.

When employing water as the active hydrogen-containing compound in the process of the present invention there is a strong preference to conduct the telomerization reaction in the presence of carbon dioxide; very good results having been obtained when CO₂ is present in an amount which corresponds with a CO₂ pressure in the range of from 500 to 5000 kPa.

When in the process of the present invention a primary or secondary amine is used as the active hydrogen – containing compound, it is preferred that the diphosphine is a bis(dialkylphosphino) based diphosphine and especially a bis(di – n – butylphosphino) or bis(diisopropylphosphino) based diphosphine. On the other hand when water is employed as the active hydrogen – containing compound, both bis – (diarylphosphino) and bis(dialkylphosphino) based diphosphines have resulted in a high conjugated diene conversion and a high selectivity to the linear alcohol type reaction product.

The process of the present invention will generally be conducted at a temperature in the range of from 20 to 180 °C and preferably in a range of from 50 to 150 °C.

The pressure at which the present invention is conducted will generally be in the range of from atmospheric pressure to 10000 kPa, taking in account of course the hereinbefore mentioned preferred presence of carbondioxide when employing water as the active hydrogen – containing compound.

The telomerization products prepared can be recovered for example via fractionation, distillation and/or crystallization, and may advantageously be employed as such or used for example for the synthesis of polymers, synthetic resins, epoxy compounds and surface – active agents.

When water is the active hydrogen – containing compound, the telomerization product (dienol) can be hydrogenated to the corresponding alcohol and subsequently dehydrated to the corresponding alkene. For example, product 3,7 – diene – octanol can be hydrogenated to octanol and subsequently dehydrated to 1 – octene.

The invention will be further illustrated with the following examples which should however not be considered as limiting the scope of the invention or the manner wherein it may be practised.

The following information is provided for the examples and comparative experiments:

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	Di- and	monophosphines used in Tables I and II
	Code	Phosphine type
5	a)	1,3-bis(di-n-butylphosphino)propane
	b)	1,3-bis(diphenylphosphino)propane
	c)	1,2-bis(diphenylphosphino)ethane
	d)	1,3-bis(diisopropylphosphino)propane
10	e)	1,4-bis(diphenylphosphino)butane
	f)	1,4-bis(di-n-butylphosphino)butane
	g)	triphenylphosphine
15		
		Amines used
20		p) n-butylamine

q)

Example I 25

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Into a 250 ml stainless steel (Hastelloy C) autoclave equipped with a magnetic stirrer were introduced 0.25 mmol Pd(OAc)₂, 0.37 mmol 1,3 - bis(di - n - butylphosphino)propane (a), 40 ml anisole and 10 ml n butylamine. Subsequently the reactor was closed and the air evacuated therefrom, whereupon 10 ml 1,3 butadiene were introduced, and the reactor contents heated to 125 °C, which temperature was maintained for 5 hours. Subsequently the reactor contents were cooled to 20 °C. Analysis by gas liquid chromatog raphy (g.l.c.) indicated that 56% of the butadiene had been converted to a mixture of N – (octadienyl – 2,7) – n – butylamine(53%), N,N-di-(octadienyl-2,7)-n-butylamine(29%)octatriene - 1,3,7(24%).

diethylamine

Examples II - V

The procedure of Example I was repeated with the exception of a change in diphosphine and/or a replacement of the 10 ml of n-butylamine with 15 ml of diethylamine and/or a change in the reaction temperature, as has been indicated in Table I, which Table also presents the product data obtained.

Comparative experiments A and B

The procedure of Example I was repeated with the exception that 1,3 - bis(diphenylphosphino)ethane (c) was used as ligand, while in experiment A the reaction temperature was 135 °C and in experiment B 15 ml of diethylamine were employed. The process details and product data have been included in Table I.

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5	•	on triene %	24	30	80	5	7		25	(-1:1)
10	1	Product composition mine tert.amine triene % %	29	12	06	95	92		20	traces
15	1	Produsec.amine	53	20	•		•		20	
20	Table I	Butadiene conversion %	99	25	25	78	93		20	< 5
25		Temp °C	125	125	135	100	100		135	125
30		Amine type	ď	ď	o'	ט	ъ		Q.	ם :
35		Phosphine type	ct ct	٩	Ą	æ	þ		ပ	U
40		Ехатр1е	I	11	111	IV	>	Comp. exp	A	В

5 Examples VI – X

To an autoclave of the type as described in Example I was added, 0.25 mmol Pd(OAc)₂, 0.37 mmol of a diphosphine as indicated in Table II hereinafter, 5 ml water and 40 ml diglyme.

After closing the reactor and evacuating the air therefrom, 10 ml of 1,3 – butadiene were added which was followed by pressurizing the reactor with carbondioxide to a pressure corresponding with the value indicated in Table II. The reactor contents were heated to 110 °C and maintained at this temperature for 5 hours. Subsequently the reaction contents were cooled to 20 °C and analyzed via g.l.c. Reaction details and product data have been collected in Table II.

Comparative experiments C - E

The procedure of Examples V-X was repeated with the exception that 1,2-bis(diphenylphosphino) - ethane (c) (0,37 mmol) or triphenylphosphine (g) (0,7 mmol) was used as the phosphine compound.

Process details and the corresponding product data have been included in Table II.

From the results obtained in Examples I to V (Table I) and those obtained with the comparative experiments A and B, it can be observed that the use of diphosphines having at least 3 atoms in the bridge as described hereinbefore, and especially the bis(dialkylphosphino) based diphosphines can result in very high conjugated diene conversions in combination with a high selectivity to the telomerized products.

A similar phenomenon can be observed when comparing the results of Examples VI-X (Table II) with those of comparative experiments C and E.

Finally it can be concluded that as the catalyst systems of the process of the present invention are based on chelating ligands, they will be more stable than the corresponding systems based on mon-ophosphines.

		triene	dΡ	22	12	20	25	30		-45	30	07	• • • •
10		t composition secondary alcohol	фP	7	9	7	9	9		~5	12	6	
15		2											
20		Produ primary alcohol	dΡ	02	80	71	<i>L</i> 9	61		~50	55	67	
25	Table II	Butadiene conversion	ф	88	92*	85	92	06		5	95	85	medium included 10 ml triethyl amine
30		Temp °C		110	110	110	110	110		110	110	110	0 ml tr
35		co_2 pressure	kPa	1000	2000	1000	1000	1000		2000	2000	1000	included l
40		Phosphine type		• • • • • • • • • • • • • • • • • • •	ಣ	٩	Ð	44		ပ	ы	60	
45		Example		IA	VII	VIII	XI	×	Comp. exp.	U	Q	ធា	* The reaction

Claims

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1. A process for the telomerization of conjugated alkadienes which comprises contacting a conjugated alkadiene with a compound having at least one active hydrogen atom, in the presence of a catalyst obtainable from a palladium compound and a diphosphine of general formula R¹R²PRPR³R⁴, wherein R is a bivalent organic bridging group containing at least 3 atoms in the bridge, of which at least two are carbon atoms; R¹,R²,R³ and R⁴ are the same or different and represent optionally polar substituted

hydrocarbyl groups.

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- 2. A process as claimed in claim 1, wherein the bridging group R is an alkylene group containing from 3 to 5 carbon atoms in the bridge.
- 3. A process as claimed in claim 1 or 2, wherein R¹,R²,R³ and R⁴ are the same and respresent an aryl group or an alkyl group having up to 10 carbon atoms and preferably from 2 to 5 carbon atoms.
- 4. A process as claimed in any one of claims 1 to 3, wherein the diphosphine is selected from the group consisting of 1,3 bis(diphenylphosphino)propane, 1,4 bis(diphenylphosphino)butane, 1,3 bis (diisopropylphosphino)propane, 1,3 bis(di n butylphosphino) propane and 1,4 bis(di n butyl phosphino)butane.
- 5. A process as claimed in any one of claims 1 to 4, wherein the palladium compound is a palladium carboxylate and preferably palladium acetate.
 - 6. A process as claimed in any one of claims 1 to 5, wherein the diphosphine is present in a ratio of from 0.2 to 10 and preferably in a ratio from 0.5 to 5 mol per gram atom of palladium.
- 7. A process as claimed in any one of claims 1 to 6, wherein the palladium compound is employed in a ratio in the range of from 10⁻⁶ to 10⁻¹ and preferably from 10⁻⁵ to 10⁻² gram atom of palladium per mol of conjugated alkadiene.
 - 8. A process as claimed in any one of claims 1 to 7, wherein the alkadiene is 1,3 butadiene.
 - 9. A process as claimed in any one of claims 1 8, wherein the active hydrogen containing compound is water, and which is conducted in the presence of carbon dioxide.
- 10. A process as claimed in any one of claims 1 9, wherein the active hydrogen containing compound is a primary or secondary amine and the diphosphine is a bis(dialkylphosphino) based diphosphine and preferably a bis(di n butylphosphino) or a bis(diisopropylphosphino) based diphosphine.
- 11. A process as claimed in any one of claims 1 to 10, which is conducted at a temperature in the range of from 20 to 180 °C and preferably in a range of from 50 to 150 °C, and at a pressure in the range of from atmospheric pressure to 10000 kPa.

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EP 92 20 3452

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	The present search report has b	een drawn up for all claims				
	Place of search	Date of completion of the search	- 	Econolog		
TI	HE HAGUE	26 FEBRUARY 1993	V	RIGHT M.W.		
X : partic Y : partic docur A : techn	ATEGORY OF CITED DOCUME cularly relevant if taken alone cularly relevant if combined with an ment of the same category sological background written disclosure	E : earlier patent do after the filing d	cument, but publis ate in the application or other reasons	hed on, or		